



PROCESS MODELING OF THE CO-CURE OF HONEYCOMB CORE SANDWICH STRUCTURES

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Project Overview



Physics-Based Modeling of the Co-Cure of Honeycomb Core Sandwich Structures

Long-Term Goal

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Develop a physics-based model that allows assessment and optimization of co-cure for aerospace structures

Additional Goals

- Clarify and expand the community's understanding of co-cure processes
- Develop diagnostic tools that enable process analysis and optimization
- Produce guidelines for successful co-cure of honeycomb sandwich structures



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Timeline



	WORK PACKAGE		YEAR 1				YEAR 2			YEAR 3			YEAR 4				
Phase I	WP1																
	1.1 Prepreg	\checkmark	\checkmark	\checkmark	\checkmark	Μ	1.1 🗸										
	1.2 Film Adhesive	\checkmark	\checkmark	\checkmark	\checkmark	М	1.2 🗸										
	1.3 Honeycomb Core (E+M)	\checkmark	\checkmark	M1	.3 🗸												
	WP2																
	2.1 Governing Equations	\checkmark		М	2.1												
	2.2 Lab-Scale Studies	\checkmark	М	2.2													
Phase II	WP3																
	3.1 Numerical Implementation			\checkmark			M3	.1									
	3.2 Lab-Scale Studies									\checkmark	\checkmark						
	3.3 Demonstrator Studies													MB	.2		
	WP4																
	4.1 Model Refinement															M	4.1
	4.2 Demonstrator Studies																

M3.1 Implement governing equations within numerical process simulationM3.2 Validate numerical process simulation using demonstrator case studies







Today's Update



- Model Development Facesheet Consolidation
 - Modeling update
 - Validation details
- Model Development Permeability
 - Modeling update
- Next Steps Thoughts
 - Porosity modeling
 - Model integration
 - Material implementation
 - Validation





Consolidation Problem









- Resin Flows Relative to Fiber Bed
- Volatiles Move Relative to Fiber Bed
- Volatiles Move Relative to Resin (Mobility Tensor U)
- Volatiles Dissolve in Resin
- Volatiles Diffuse, Too



• Fiber Bed with Resin and Porosity f

- Fiber Volume Fraction
- *v_f* Reference Frame Fixed to Fiber Bed
- Dissolved Volatiles Concentration c

Strain e

Fiber Bed Deforms with

(Linear Strain May Suffice)







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ASSUMING INSTANT DISSOLUTION : $c = K_h p$

THE EQUATIONS FOR DISPLACEMENT, RESIN PRESSURE AND POROSITY ARE

Momentum

$$E_{r}.u' - E_{t}\frac{u}{r} + r(E_{r}.u' - p)' = 0$$
Resin Conservation

$$\frac{\partial u/\partial t}{r} + \frac{\partial u'}{\partial t} - \frac{\partial \varphi}{\partial t} = \frac{1}{r}\left(r\left(\frac{K}{\eta}p'\right)\left(1 - \frac{\varphi}{1 - v_{f}}\right)\right)'$$
P_c
Volatile Conservation

$$m_{m}\frac{\partial\left(\frac{p\varphi}{RT}\right)}{\partial t} + \frac{\partial\left(K_{h}\rho p(1 - v_{f} - \varphi)\right)}{\partial t} = \frac{1}{r}\left(rU\frac{K}{\eta}p'm_{m}\frac{p\varphi}{RT}\right)' + \frac{1}{r}(rJK_{h}p')'$$







- SOLVE FOR CONVENTIONAL COMPACTION WITHOUT POROSITY FOR CONSTANT MATERIAL PROPERTIES (FULLY IMPLICIT)
 - FIRST TWO EQUATIONS ONLY
- ADD VARIABLE MODULI AND PERMEABILITY USING EXPLICIT CONSTANTS
 WITHOUT POROSITY TRANSPORT
 - FIRST TWO EQUATIONS ONLY
- ADD POROSITY TRANSPORT BY STAGGERED SOLUTION AND EXPLICIT CORRECTION FACTOR IN PREVIOUS SOLUTION
 - IN PROGRESS









Linear Case

$$\begin{bmatrix} u \\ p \end{bmatrix}^{n+1} = K^{-1} \cdot F\left(\begin{bmatrix} u \\ p \end{bmatrix}^n \right)$$

F is Linear

$$\begin{bmatrix} u \\ p \end{bmatrix}^{n+1} = K^{-1} \left(\begin{bmatrix} u \\ p \end{bmatrix}^n \right) \cdot F \left(\begin{bmatrix} u \\ p \end{bmatrix}^n \right)$$

u: Radial Displacement p: Resin Pressure

Without Porosity Transport

Linear Material Allows Implicit Formulation.

Non-Linear Material and 1st Order Euler Time Stepping Suitability (No Real Time Step Limits):

- 1. Kožený Karmán Permeability
- 2. Linear Modulus of Elasticity
- 3. Non-Linear Modulus of Elasticity by Gutowski (Sandwich)

The Same with TVD-RK3 Time Stepping

1. Quadratic Modulus of Elasticity Works Without Time Limits

Non-Linear Approach Does Not Work (Or with Unbearable Time Limits):

1. Cubic Modulus of Elasticity





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Theoretical Stress-Strain Curve(s)



Notes: 1. Compaction Work at UD Involved Glass Preforms 2. Higher Non-Linearity Complicates Numerics

Measured Stress-Strain Curve





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Sample Panel Comparison Details: Material Model



- Prepreg Data Came from Different Material
 - Low Pressure (We went to 377 kPa in Comparison Panels)
 - More Modest Fiber Content (53-59%)
- Fit Modified to Stress-Strain Form
 - Works OK in the Code as Is
 - Non-Linearity not Very Strong
 - Similar to Linear Modulus Dependency
 - May be OK for Co-Cure as the Pressure is Limited













Thickness=2 mm Outer Radius = 15 mm Tangential Modulus = 1 Gpa Transverse Modulus Nonlinear Fiber Volume Fraction ~ 0.53 Permeability 1x10⁻¹⁴ m², Kozeny-Karman Viscosity = 10 Pa.s

Applied Pressures

	Case 1	Case 2	Case 3
P _{bag}	O kPa	101 kPa	239 kPa
P _{app}	377 kPa	377 kPa	377 kPa
P _{core}	0 kPa	101 kPa	239 kPa

Notes

- Viscosity Could Be Used Transient, But this is Good "Representative" Value
- Tangential Modulus (Prepreg In-Plane Stretching) is Speculative
- Permeability is "In Ball Park"
- Kozeny-Karman is Commonly Used as It Needs Only One Data Point
- Radius Obtained From Expected Dimpling







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Comparison Details: Good Qualitative Agreement







Is the Solubility the ONLY Key?







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Comparison Details: Reasonable Qualit. Agreement







No Clear Trend in the Experiment Are Voids "Toward" Core?!



Low Resin Pressure







Gas Transport Experiments (Controlled Conditions)

- Variables
 - Ply count
 - Compaction pressure
 - Resin viscosity
- Measured values
 - Gas flow rate
 - Facesheet thickness?
- Other considerations
 - Boundaries: release film, adhesive layer
 - K_x, K_y
 - Material: 8552, 5320-1?

Fitting to Standalone Model









Technical Questions



Equilibrated Core

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- How can we improve the accuracy of <u>porosity</u> modeling?
 - Void nucleation (currently not considered)
 - Void growth (reasonable first-pass agreement)
 - Void rupture and/or migration (highly stochastic)
- Is the <u>coupling</u> between facesheet consolidation and bond-line formation essential for predictive modeling?
 - Resin bleed can lead to thicker bond-line, larger fillets, and more porosity
- Is the model accurate for <u>OoA/VBO prepregs</u> with low degrees of impregnation?
- What are the next steps for <u>validation</u>?

Sealed Core

- How do we develop an accurate but useable model for prepreg permeability during cure?
- How do we reconcile prepreg permeability and facesheet consolidation?





Porosity Formation





Next Step: Growth/Shrinkage Transition

- Models can be developed for adhesive and prepreg resins. \succ
- Prediction of growth/shrinkage transition can be validated \geq and used to estimate bond-line quality.



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Experimental Data

- In situ visuals
- Vacuum oven (mass loss)
- Void growth/shrinkage
- Void nucleation (if needed)

Current State

Model predicts transition at approximately 100 kPa (for adhesive). Tests show that voids in bond-line require > 200 kPa to suppress.





Facesheet/Bond-Line Coupling



	Visual Observations	Fillet Formation	Notes
	<u>In Situ</u> : Fillet formation, little void growth	<u>Measured</u> : Fillet height measured for approx. 40 fillets, with large STDEV noted	Simple analytical model over- predicts fillet height, but remains accurate to within about 15%
CASE	Polished Section: Fillets are well-formed, few/no voids	Model: Analytical model solved using known/assumed parameters	 (average). ➤ To account for resin bleed, the model peeds to be revised.
an a filo an an anti a tha an a' a da an a		Model Results:	Resin mass as input
	<u>In Situ</u> : Fillet formation, void growth and entrapment	 Sources of error: void formation, carrier, resin bleed from prepreg 	 Multiple material properties Time history dependence
CASE	Polished Section: Large fillets, many entrapped voids	1.2	How accurate does the prediction of fillet size need to be, given practical factors and variability?
	<u>In Situ</u> : Fillet formation, void growth/rupture		
CASE	Polished Section: Small, irregular fillets with some entrapped voids	0.2 0 Vacuum Ambient Pressurized	
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OoA/VBO Prepreg



Autoclave

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- Fiber bed is fully saturated with resin on delivery.
- Consolidation modeling is easier due to uniformity.
- ➢ <u>Material</u>: Hexcel 8552S

Out-of-Autoclave

- Fiber bed is not fully saturated with resin due to dry tows
- Consolidation modeling is more challenging due to partial saturation, non-uniformity
- Material: Cytec 5320-1







Questions

- How accurate (or not) is the model for 5320-1?
- Can we decouple tow impregnation from the current consolidation model?
- How do we account for permeability evolution?



Validation



- **Case I:** Equilibrated Core ($P_{core} = 0$ kPa)
 - Sub-Models: Fillet formation, porosity formation
 - Focus: Current
- **Case II:** Equilibrated Core ($P_{core} = 101.3$ kPa)
 - Sub-Models: Fillet formation, porosity formation
 - Focus: Current
- **Case III:** Equilibrated Core ($P_{core} = 240$ kPa)
 - Sub-Models: Fillet formation, porosity formation
 - Focus: Current
- Case IV: Sealed Core (Realistic Pressure Evolution)
 - Sub-Models: *Cases I III + core pressure*
 - Focus: Upcoming (requires facesheet permeability)
- Cases V+: Parts with Defined Geometry
 - Sub-Models: Case IV + <u>2D geometry</u>
 - Focus: After Cases I IV are validated

Current Validation Tasks

- <u>Improve methods</u> for collecting test data (esp. for facesheet properties)
- <u>Refine models</u> (equations, inputs) to improve accuracy of fillet formation, porosity evolution, and facesheet consolidation sub-models.

Next Steps

- Prepare additional samples to assess variability.
- Perform validation on external samples
- (e.g., UTRC test data).



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